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POLYCARBONATE/POLYPROPYLENE-GRAFT-MALEIC ANHYDRIDE AND NANO-ZEOLITE-BASED NANOCOMPOSITE MEMBRANE: MECHANICAL AND GAS SEPARATION PERFORMANCE

ABSTRACT

In this effort, blend membrane of polycarbonate (PC) and polypropylene-*graft*-maleic anhydride (PPMA) was fabricated *via* phase inversion technique. The nano-zeolite (NZ) was employed as nanofiller. Morphology of PC/PPMA/NZ membrane revealed unique inter-connected branched microstructure. Tensile strength and Young's Modulus of PC/PPMA/NZ 0.1-5 were in the range of 59.9-74.5 MPa and 111.4-155.2 MPa respectively. The nano-zeolite filler was also effective in enhancing the permselectivity $\alpha_{\text{CO}_2/\text{N}_2}$ (23.5 to 38.5) relative to blend membrane (20.3). The permeability P_{CO_2} of PC/PPMA/NZ 5 membrane was found as 106.2 Barrer. Filler loading enhanced gas diffusivity, however filler content did not significantly influence CO_2 and N_2 solubility.

Keywords: *Polycarbonate, nano-zeolite, permselectivity*

INTRODUCTION

Generally, polymer blends are physical mixture of structurally different polymers. The polymeric blends have distinct potential benefits owing to physical and structural properties. In thermodynamic stance, most of the polymers are immiscible. However, miscible polymer blends may engender high performance materials with unique properties and processability. Polymer blends have been prepared using variety of engineering resins and techniques, focusing wide range of applications [1, 2]. As polymer blends are multi-phase systems, they may form different morphological structures such as fibres, spheres, ribbons, plates, cylindrical and other structures. The blend morphology can be varied *via* inclusion of nanoparticle such as silica, zeolite, carbon nanotube, and other nanofiller. One of the most widely used thermoplastic polyolefin is polypropylene (PP). It has been considered for compositing intended for the production of new nanocomposite. The maleic anhydride grafted polypropylene has been employed as compatibilizer for the production of nanocomposite [3, 4]. In this case the morphology and characteristics of final material may be varied by density of maleic anhydride groups [5]. Another important class of thermoplastic polymers is polycarbonate (PC) [6]. Polycarbonate has been considered between the commodity plastics and engineering plastics. Its chemical structure consists of carbonate group. Polycarbonate is

strong and tough; however it is easily workable, moldable, and thermo-formed. PC has fine mechanical properties such as impact and shock resistance [7]. The glass transition temperature of polycarbonate is found ~ 150 °C. Moreover, polycarbonate has fine optical properties and thermal resistance [8]. Zeolite is considered as significant polymer filler/nanofiller. It may form micro-porous crystals with complex channels and pores. Furthermore, it is frequently exploited as an ion-exchanger, adsorbents, and catalysts [9, 10]. The size of zeolite particles may be influenced by crystallization at controlled temperature [11]. Zeolite has potential application in separation membranes due to fine adsorption and diffusion selectivity. Polycarbonate membranes reinforced with zeolite are exceptionally permeable and selective. High performance zeolite-based membranes have been achieved with easy processability, sorption characteristics, and shape selectivity of nanoparticles. Increasing zeolite content may act as adsorbing component in the membrane [12-14]. Moreover, high potential polycarbonate/zeolite mixed matrix membrane has also been developed [15]. The membrane structure and performance have been influenced by the particle size and zeolite content. Solvent evaporation methodology is commonly used for these membranes. Melt compounding has also been employed as preferred technique [16-18]. According to morphology investigation, zeolite may form large clusters in polycarbonate membrane. Moreover, permeability of PC membranes has been found to decrease with zeolite loading. Nevertheless, improvement in selectivity was observed for PC/zeolite membrane relative to neat polycarbonate membrane [19, 20]. The zeolite strengthened polyimide and polysulfone membranes have been developed and investigated [21, 22]. Effect of surface modification of zeolite on the physical properties of polyimide hybrid films was also investigated [23, 24]. Mechanical stability of the membranes was found to increase with zeolite loading. In this attempt, nano-zeolite-based nanocomposite membranes have been developed for CO₂/N₂ separation. A blend of polycarbonate (PC) and polypropylene-*graft*-maleic anhydride (PPMA) was designed in this regard. The nano-zeolite reinforced PC/PPMA blend membranes possess fine CO₂/N₂ gas-separation performance and mechanical properties relative to neat blend membrane.

EXPERIMENTAL

Materials

Polypropylene-*graft*-maleic anhydride ($M_w \sim 9,100$, $M_n \sim 3,900$, maleic anhydride 8-10 wt.%), polycarbonate (PC, $M_w \sim 50,000$), zeolite (<10 μm), and dimethylformamide (DMF, 99%) were obtained from Aldrich.

Measurement

The average size of particles was also determined by dynamic light scattering method (DLS) (LPA 3000 Photol, Otsuka Electronics). Fourier transformed infrared (FTIR) spectra were recorded in the range of 400-4000 cm^{-1} using a Perkin-Elmer FTIR spectrometer. Field Emission Scanning Electron Microscopy (FE-SEM) was performed using JSM5910, JEOL Japan to examine freeze-fractured samples. Tensile tests of all the samples were performed using Shenzhen Sans Universal Testing Machine (UTM), at ambient conditions with cross head speed of 2 mm/min and 0.5 kN load. Gas permeation tests were performed at 27 °C and upstream pressure of 10 psi [25]. The value of gas permeability (P) was measured from Eq (1):

$$P = \frac{VL}{ART\Delta P} \frac{dP}{dT} \quad (1)$$

Where:

V = downstream volume

L = membrane thickness

A = membrane area

R = universal gas constant

T = absolute temperature

$\Delta P = p_2 - p_1$ = Trans membrane pressure difference; p_2 and p_1 upstream and downstream pressures

dp/dt = steady rate at which pressure increases on the downstream side.

The permselectivity (α) was calculated using Eq (2):

$$\alpha = \frac{P_A}{P_B} \quad (2)$$

Where:

P_A and P_B are permeabilities of two gases

The diffusivity (D) was estimated from Eq (3):

$$D = \frac{L^2}{\theta} \quad (3)$$

Where:

θ = time lag when a steady dp/dt rate is obtained on the downstream side

L = membrane thickness

The solubility (S) was determined from Eq (4):

$$S = \frac{P}{D} \quad (4)$$

D = diffusivity

P = permeability

Nano-zeolite formation (NZ)

Nano-zeolite was prepared using ball milling process. Zeolite powder, as obtained from Aldrich, was used for ball milling. For this purpose, ball to powder ratio was kept as 10:1. Crushed nano-zeolite powder was obtained after 96 h of ball milling. The powder further employed as nano-filler [26]. The average nanoparticle size determined by DLS was 75 ± 0.1 nm.

Polycarbonate/polypropylene-graft-maleic anhydride (PC/PPMA) membrane formation via phase inversion

The 0.3g PC was dissolved in 1 mL DMF via 3 h sonication. A dispersion of 0.2g PPMA was also prepared in 0.5 mL DMF with sonication of 2h. The PPMA solution was then added to the PC solution. The mixture was refluxed for 2h at 80 °C. The solution was cast on glass plate using knife. The glass plate was then immersed in aqueous solution for 0.5 h. The resulting membranes were dried at 80 °C for 2h [27].

Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite membrane(PC/PPMA/NZ)

The phase inversion route was also used for the formation of composite membranes. 0.3g PC and 0.2g PSAA was dissolved in DMF. To the mixture, desired content (1-10 wt.%) of nano-zeolite were added (Fig. 1). The membrane composition is given in Table 1.

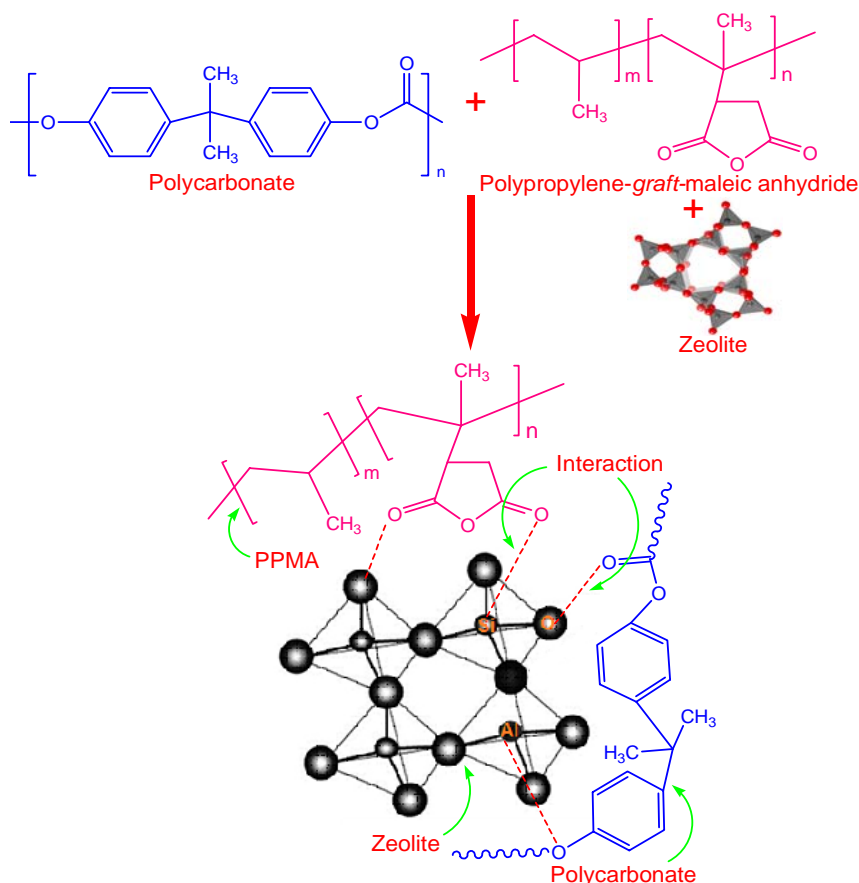


Fig. 1. Formation of polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite membrane

Table 1. Sample codes and composition used

Sample	Composition	PC	PSAA	NZ (wt.%)
PC/PPMA	Polycarbonate/polypropylene-graft-maleic anhydride	0.3	0.2	0
PC/PPMA/NZ 0.1	Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite 0.1	0.3	0.2	0.1
PC/PPMA/NZ 0.5	Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite 0.5	0.3	0.2	0.5
PC/PPMA/NZ 1	Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite 1	0.3	0.2	1
PC/PPMA/NZ 3	Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite 3	0.3	0.2	3
PC/PPMA/NZ 5	Polycarbonate/polypropylene-graft-maleic anhydride/nano-zeolite 5	0.3	0.2	5

RESULTS AND DISCUSSION

Structural analysis

FTIR spectra of PC/PPMA and PC/PPMA/NZ 1 are given in Fig. 2. In the blend spectrum, characteristic peaks of aliphatic and aromatic C–H stretching vibration appeared at 2950 and 3011 cm^{-1} (Fig. 2A). The C–O stretching vibration was found at 1230 cm^{-1} , while the carbonate C=O was located at 1689 cm^{-1} . However, the symmetric and asymmetric anhydride ring carbonyl vibrations appeared at higher frequency of 1820 and 1760 cm^{-1} respectively. The symmetric and asymmetric anhydride carbonyl vibrations were also observed (1801 and 1750 cm^{-1}) in the case of PC/PPMA/NZ 1 nanocomposite membrane (Fig. 2B). Moreover, the C=O stretch due to polycarbonate backbone was located at 1677 cm^{-1} . The peak at 1223 cm^{-1} indicated C–O stretching vibration. The shift of characteristic absorbance peaks of C=O carbonyl and C–O to lower wavenumber in PC/PPMA/NZ membrane qualitatively indicated some interaction between nano-zeolite structure and the blend matrix. In addition, the peak at 3411 cm^{-1} corresponds to inner-hydroxyl group of nano-zeolite structure. The aliphatic and aromatic C–H stretching vibration also appeared at 2901 and 3000 cm^{-1} . The peak at 1250 cm^{-1} was the characteristic of Si–CH₂ functional group. The asymmetric and symmetric Si–O stretching vibrations appeared at 1009 and 670 cm^{-1} [28]. Moreover, the peak for Si–Al–O appeared at 1030 cm^{-1} .

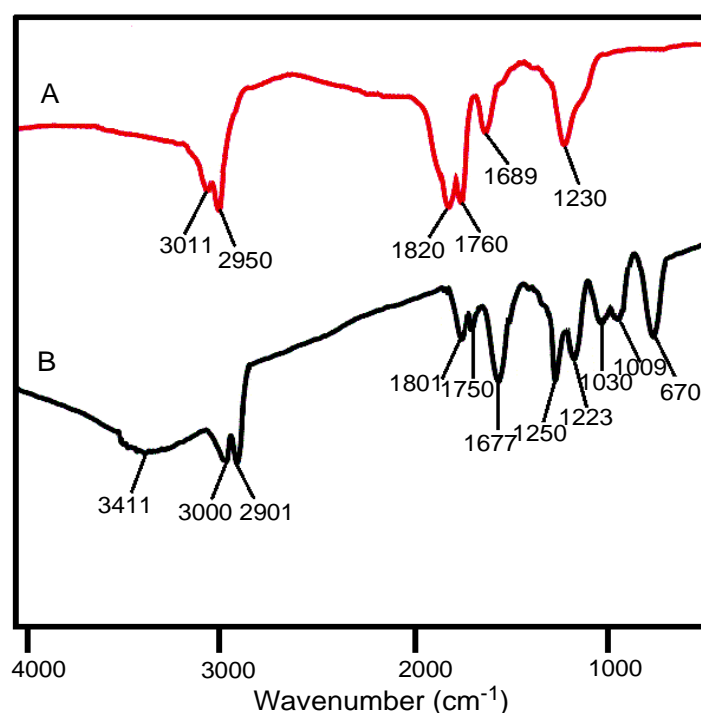


Fig. 2. FTIR spectra of (A) PC/PPMA and (B) PC/PPMA/NZ 1 membrane

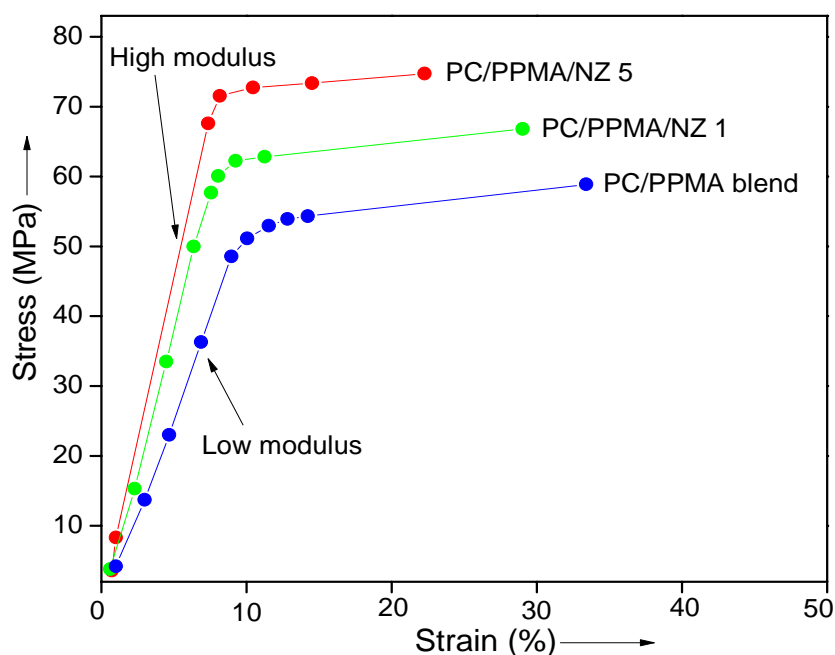
Mechanical property study

Table 2 reveals the tensile stress at break, Young's modulus, and elongation at break of PC/PPMA blend and PC/PPMA/NZ nanocomposite with various nanofiller content. In the nanocomposite membrane series, tensile strength and Young's modulus were increased with nanofiller loading, however the elongation at break was found to decrease [29, 30].

Table 2. Tensile strength, strain, and Young's modulus of PC/PPMA-based membranes

Sample	Tensile stress at break (MPa)	Elongation at break (%)	Young's Modulus (MPa)
PC/PPMA	58.4 (1.1)*	34.2 (1.3)	81.11 (1.1)
PC/PPMA/NZ 0.1	59.9 (1.2)	31.1 (1.1)	111.4 (1.3)
PC/PPMA/NZ 0.5	61.2 (1.1)	30.2 (1.2)	118.1 (1.4)
PC/PPMA/NZ 1	66.5 (1.2)	29.9 (1.2)	123.3 (1.2)
PC/PPMA/NZ 3	69.9 (1.6)	25.5 (1.2)	143.1 (1.4)
PC/PPMA/NZ 5	74.5 (1.2)	23.4 (1.1)	155.2 (1.2)

Tensile strength for neat PC/PPMA blend membrane was found to be 58.4 MPa. The strength of PC/PPMA/NZ 0.1 membrane was observed as 59.9 MPa. The property was found to increase to 61.2 MPa with 0.5 wt.% nanofiller loading. Inclusion of 1 wt.% nano-zeolite further improved the mechanical strength to 66.5 MPa. Similarly, the property was increased for PC/PPMA/NZ 3 (69.9 MPa). In this way, the tensile stress of PC/PPMA/NZ 5 was 20 % higher than the 0.1 wt.% membrane, while 22 % higher than the neat blend membrane. The higher tensile strength was observed for PC/PPMA/NZ 5 with the value of 74.5 MPa. The tensile stress results showed that the nano-zeolite addition acted as strong reinforcing agent. The mechanical property trend may be attributed to fine nano-filler orientation in the blend matrix, which significantly increased the mechanical properties of the resulting nanocomposite. The Young's modulus of PC/PPMA/NZ 0.1-5 series was increased from 111.4 to 155.2 MPa. Here, the 5 wt.% sample showed 23 % increase in Young's modulus relative to PC/PPMA/NZ 1, and 48% increase relative to neat PC/PPMA blend. The stress-strain curves of PC/PPMA blend and PC/PPMA/NZ nanocomposite membranes are given in Fig. 3.

**Fig. 3.** Stress-strain diagram of blend, PC/PPMA/NZ 1 and PC/PPMA/NZ 5 membrane.

The results also suggested decrease in the elongation at break of PC/PPMA/NZ 0.1-5 from 31.1 to 23.4%. Neat blend had higher elongation at break value of 34.2%. The zeolite nanofiller acted as interesting and promising reinforcing filler for the nanocomposite membranes. Accordingly, the membrane performance and latent in technological applications has been fundamentally improved.

Morphology investigation

The surface morphology of PC/PPMA blend and PC/PPMA/NZ membranes at micrometer length scale is given in Fig. 4.

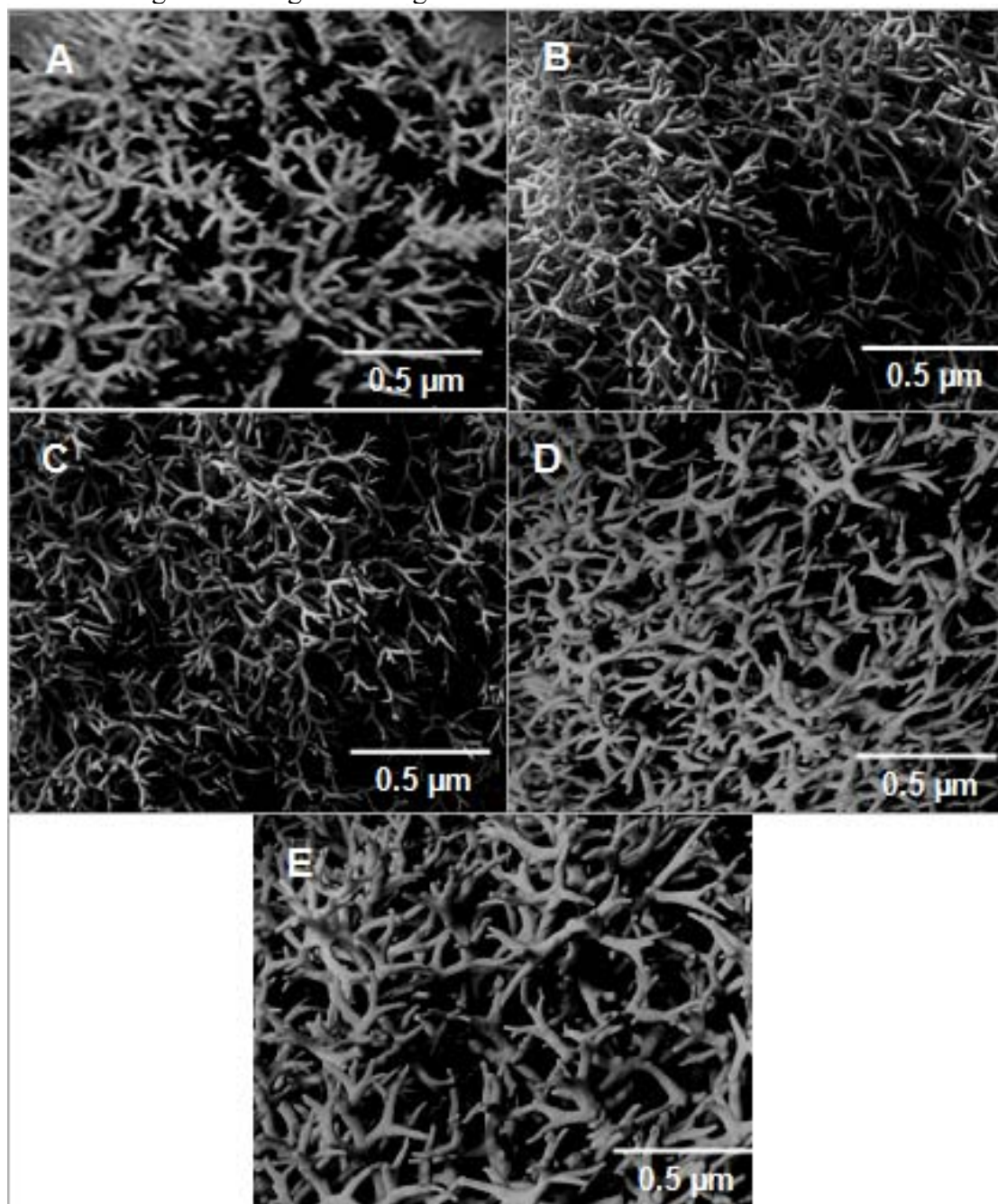


Fig. 4. FESEM images of (A) PC/PPMA blend; (B) PC/PPMA/NZ 0.5; (C) PC/PPMA/NZ 1; (D) PC/PPMA/NZ 3; and (E) PC/PPMA/NZ 5

Assessment of the fractured surface of PC/PPMA blend revealed unique branched and entangled morphology of the two phases (Fig. 4A). It seems that the polycarbonate formed continuous phase (the matrix) in which the polypropylene-*graft*-maleic anhydride second phase was dispersed in some pattern. In PC/PPMA/NZ 0.5 membrane, however the nano-zeolite filler content was so small; the morphology was altered with the formation of fine inter-connected branched nano-pattern (Fig. 4B). The nano-zeolite particles were not observed on the fractured surface. It seemed that the nanofiller was merged in the PC/PPMA blend. In PC/PPMA/NZ with 1 wt.% nanofiller, the pattern showed further small branching, however the pattern was diffused at certain placed in the matrix (Fig. 4C). In PC/PPMA/NZ with 3 wt.% nano-zeolite, the morphology attained a fine pattern due to increased filler content and better dispersion (Fig. 4D). The PC/PPMA blend formed dense pattern with somewhat elongated branches in the structure. The most finely branched and entangled pattern was observed in the case of PC/PPMA/NZ 5. Branching was again dense with the protuberated fibrils at the fracture surface (Fig. 4E). The formation of unique interconnected branched microstructure indicated fine interaction and alignment between the blend matrix and nano-zeolite. This type of morphology is unique in the case of polycarbonate and zeolite blend membranes.

Gas separation performance of PC/PPMA and nano-zeolite-based membrane

Generally, gas permeability is affected by nanofiller distribution and matrix/nanofiller alignment [31, 32]. The permeability and permselectivity of PC/PPMA-based nanocomposite membrane as a function of filler concentration is given in Table 3. The PC/PPMA blend has permeability PCO_2 of 177.2 Barrer and permselectivity α_{CO_2/N_2} of 20.3. The membrane with 1 wt.% filler revealed permeability PCO_2 of 173.1 Barrer and permselectivity α_{CO_2/N_2} of 23.5. The CO_2 permeability of PC/PPMA-based nanocomposite membrane was increased with increasing the filler concentration. The α_{CO_2/N_2} of PC/PPMA/NZ 5 membrane reached 38.5 at 5 wt.% filler content i.e. the permselectivity was 38% increased with respect to 0.1 wt.% sample and 47% increased relative to the blend sample. However, PCO_2 of PC/PPMA/NZ 0.5 membrane was 170.5 Barrer, which was further decreased to 162.2 Barrer in PC/PPMA/NZ 1 membrane.

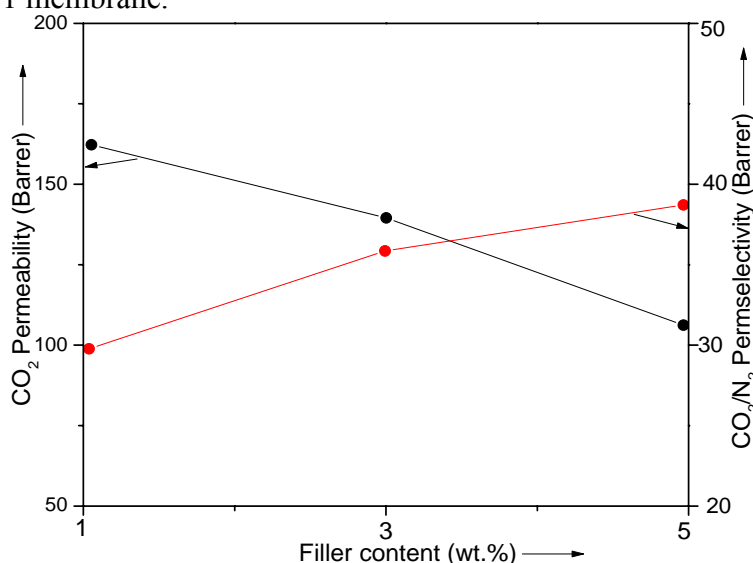


Fig. 5. Permeability and permselectivity of PC/PPMA/NZ nanocomposite membranes as a function of filler content

The 5 wt.% nano-zeolite loaded PC/PPMA/NZ 5 showed PCO_2 of 106.2 Barrer i.e. the permeability was decreased. In this way, the permeability PCO_2 of nanocomposite membrane was several fold decreased with the nanofiller addition. It seems that the NZ was found more effective than the nano-zeolite in enhancing the permselectivity and decreasing the CO_2 permeability (Fig. 5). Further scrutiny suggested that the CO_2 and N_2 diffusivity was also increased with the nanofiller loading in the membranes. Fig. 6 shows that the N_2 and CO_2 diffusivity of the 5 wt.% nanocomposite membrane was found higher than the blend membrane. Moreover, the nanofiller content did not significantly influence the CO_2 and N_2 solubility in the PC/PPMA/NZ membranes [33]. The overall results suggest that the adding nano-zeolite improved the gas separation properties rather than deteriorating them. Fig. 7 shows a proposed model for surge of gas molecules through of zeolite-filled membrane. The mass transport through a zeolite layer is qualitatively imagined by a four step model [34, 35]. Four steps are expected to involve including (i) adsorption: from gas phase to membrane surface; (ii) mass transport: from surface to zeolite pores; (iii) intra-zeolite diffusion; and (iv) diffusion: out of zeolite pores to membrane surface.

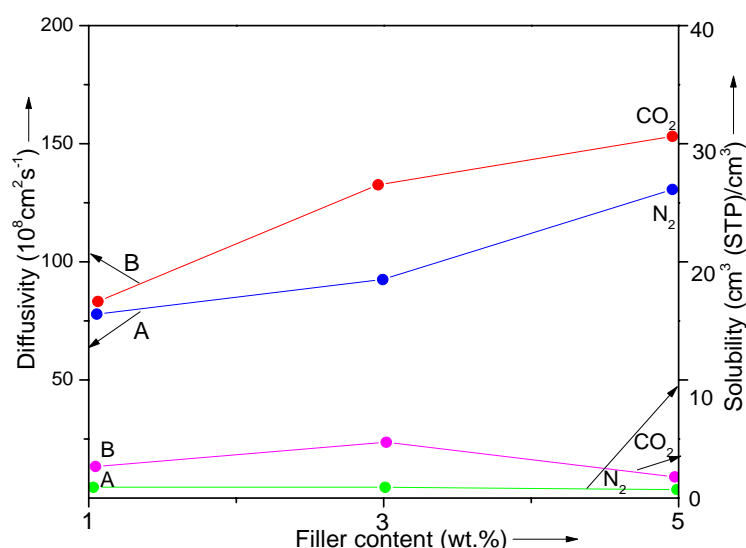


Fig. 6. CO_2/N_2 separation performance in terms of diffusivity and solubility for PC/PPMA/NZ nanocomposite membranes as a function of filler concentration.

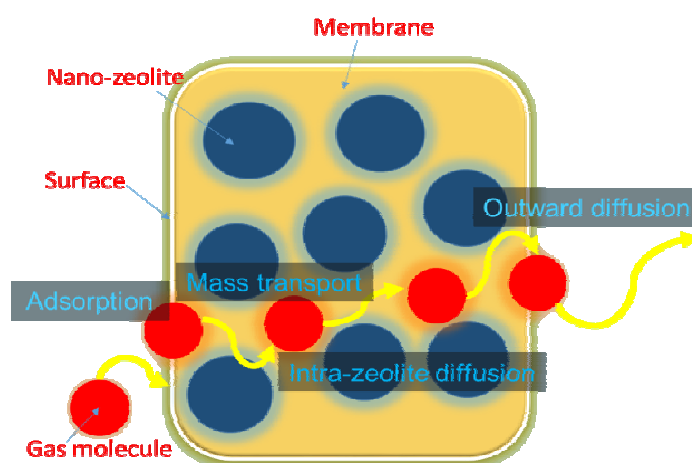


Fig. 7. Model for surge of gas molecules through zeolite membrane

CONCLUSIONS

The nano-zeolite membranes impregnated with polycarbonate/polypropylene-*graft*-maleic anhydride possesses fine morphology due to better compatibility and interaction of nanofiller with the polymer blend. Nano-zeolite content was varied between 1 to 5 wt.%, for a selected blend composition. The nano-zeolite was found to enhance the tensile strength and modulus of nanocomposite membranes, relative to the blend membranes. The tensile stress of 5 wt.% nanofiller-based PC/PPMA/NZ 5 was found to be 22 % higher than the neat blend membrane. Alternatively, the elongation at break was found to decrease. The CO₂ permeability of PC/PPMA/NZ 1-5 membrane was decreased from 177.2 to 106.2 Barrer. High NZ concentration (5 wt.%) enhanced the CO₂ selectivity $\alpha_{\text{CO}_2/\text{N}_2}$ to 38.5. Moreover, the gas diffusivity of PC/PPMA/NZ 1-5 membrane was found higher than that of blend membrane. Conclusively, better mechanical properties of polycarbonate blend membranes can be achieved, without deteriorating the gas separation performance, through the addition of nano-zeolite filler.

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